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Photo-Fenton Process: Degradation of Drimaren Red CL-5B Dye and Ecotoxicity Study of Jeans Laundry Effluent

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ABSTRACT

The textile industry is a field which has strong environmental impacts due its high consumption of water and emission of pollutants, specially the dyes. The dyes are organic or synthetic substances which alter the physicochemical characteristics of the water body in which they are released, increasing the toxicity, reducing the oxygen and light, intensifying the color and turbidity, and depleting aquatic life. The reduction of the ecotoxicological effects of the subproducts and the efficiency of treatment are points that still need much improvement. Research has shown that most dyes are resistant to conventional treatments, requiring the use of alternative treatments, as advanced oxidation processes. The aim is to evaluate the efficiency of applying the photo-Fenton process, with sunlight as a polishing treatment, on an effluent of a jeans laundry; and to investigate the degradation of the Drimaren red CL-5B dye and its ecotoxicity, with lettuce seeds before and after treatment. A factorial design was used on two levels, varying time, iron and hydrogen peroxide concentrations factors. After the treatment, there was over 90% mineralization of the dye and significant reduction in the evaluated physicochemical parameters were observed, as color, turbidity and total organic carbon; as well as a great reduction in the toxicity of the effluent.

1. Introduction

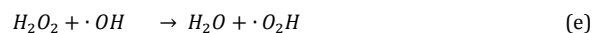
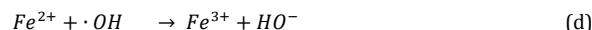
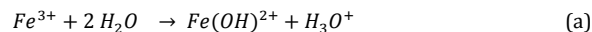
The textile industry is a complex and heterogeneous chain, comprising of the processing and production of natural and synthetic raw materials, of fabrics and of the final product delivered to consumers. The steps of bleaching, dyeing, mercerizing and washing operations consume large volumes of water: about 160 m³ per ton of fiber processed [1]. Consequently, large volumes of waste water and solid waste are generated. The need to treat the effluent waste to avoid damaging the environment, and reduce the water consumption and costs associated with production, makes it imperative to implement water reuse and management practices for this waste [2]. A basic characteristic of textile effluents is the presence of dissolved dyes that were not retained by the fibers, which generates coloration [3-5]. These are identified as the most problematic compounds in textile effluents due to their high solubility in water, organic content, high salt concentration and low degradability [3, 6-13]. The total dye production in the world is estimated at 800,000 tons/year and at least 10-15% of these are discharged into the environment through effluents [8-10].

Highly colored effluents absorb sunlight and hinder the action of photosynthetic algae. Some dyes are recalcitrant and carcinogenic and the conventional biological processes, even when in sequential anaerobic-aerobic routines, do not remove such compounds [6, 7].

The removal of colored substances from the effluent is primarily based on physicochemical methods [14]. There is no universally used method for the treatment of textile effluents, probably because of the variety of chemical structures and complexity of these compounds [15].

Several studies carried out in the past decades have shown that advanced oxidation processes (AOPs) are effective alternatives for the degradation of recalcitrant compounds, usually present in textile effluents. Photochemical processes are used to degrade toxic compounds, producing CO₂ and H₂O without using additional oxidants, as the degradation is assisted by high concentrations of a hydroxyl radical. In this case, the photo excitation of TiO₂ particles, promoted from a valence band to the

conduction band, generates the electron/vacancy pair [16]. Among the advanced oxidation processes, the heterogeneous ones with or without irradiation are used in the presence of titanium dioxide, and the homogeneous ones with or without irradiation – of which we highlight the Fenton and photo-Fenton processes. The Fenton reagent is obtained by the decomposition of hydrogen peroxide, catalyzed by the ferrous ion (Fe²⁺) in an acid medium. This decomposition forms hydroxyl radicals (•OH) which react with the pollutants causing their mineralization [17, 18]. The combination of the Fenton reagent with ultra violet radiation results in the enhanced oxidative process known as photo-Fenton. The basic characteristic of this process in relation to the Fenton process is an increased rate of degradation of the pollutants due to the use of UV radiation. The degradation rate increases because a photoreduction of Fe³⁺ to Fe²⁺ occurs as well as the photolysis of hydrogen peroxide, producing more hydroxyl radicals. The mechanism of the photo-Fenton process [19] is presented in the chemical equations (a-e), as follows:



Knowledge of the photo-Fenton reaction allows promising applications in some industrial practices at a moderate scale, and may be useful in the treatment of industrial waste and effluents [20].

The aim of this study is to evaluate the efficiency of the application of the photo-Fenton process, using sunlight, as a polishing treatment, on an effluent from a jeans laundry at Pernambuco, Brazil; and to investigate the degradation of the Drimaren red CL-5B dye, as well as the ecotoxicity, with lettuce seeds before and after treatment.

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2. Experimental Methods

2.1 Preparation of the Samples

An aqueous solution of 1,000 mg/L of the Drimaren red LC-5B dye (Clariant®) was prepared and used in the degradation study. This dye was chosen because of the demand in the industries of the region where the study was conducted. Fig. 1 shows the structure of the studied dye.

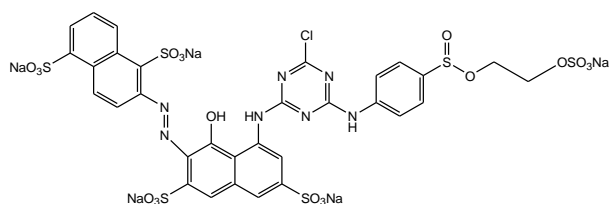


Fig. 1 Structure of the drimaren red CL-5B dye (1026.41 g.mol⁻¹) source: color index number CI: RR 241 [21]

For the ecotoxicity study of the textile effluent subjected to the photo-Fenton process, the effluent of a jeans laundry was used. The sample was collected in polyethylene containers, properly sanitized, conditioned at 5 °C and then subjected to the photo-Fenton treatment.

2.2 Analysis

The aqueous solution of the dye was subjected to photolysis processes using hydrogen peroxide with UV light and the photo-Fenton process. Artificial light was used for the tests with the solution of the dye through the bench reactor (Fig. 2), which has three fluorescent light bulbs with power of 20 W each.

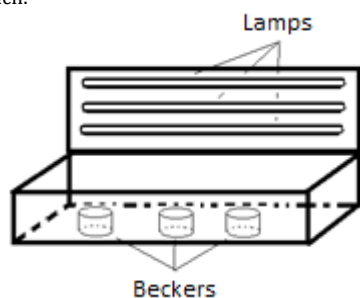


Fig. 2 Bench reactor with fluorescent bulb

The analytical curve of the dye was carried out in triplicate. The limits of quantification and detection were calculated by $LD = 3.3 \times (s/S)$ and $LQ = 10 \times (s/S)$, where s is the standard deviation of the lowest concentration response and S is the slope (angular coefficient) of the analytical curve [22–24].

The dye degradation was investigated by spectrophotometry (UV-Vis spectrophotometer Thermo Scientific Genesis 10S). The samples were analyzed before and after the photo-Fenton treatment. Dilutions were carried out using 30%, 20%, 15%, 10% and 5% of the 1,000 mgL⁻¹ solution of the dye. The linear range used for quantification of the dye was from 50 to 300 mgL⁻¹. For the real effluent, due to its complexity, scanning from 200 to 700 nm was carried out, to evaluate the degradation with emphasis on the reduction of absorption bands. Degradation percentage was determined by Eq.(1):

$$\text{Degradation \%} = \frac{[Dye]_0 - [Dye]_f}{[Dye]_0} \times 100\% \quad (1)$$

where, $[Dye]_0$ and $[Dye]_f$ are the concentrations of dye before and after treatment, respectively.

To evaluate the effect of the photo-Fenton process, a 2³ factorial design was used to determine the best degradation condition of the aqueous solution of the Drimaren red LC-5B dye. Three variables were chosen in order to verify its influence on the degradation of the dye: the reaction time when exposed to sunlight, the amount of Fe (mg) and the volume of H₂O₂. 25 mL of the aqueous solution were added to a beaker and then tests were carried out according to the plan (Table 1).

The same planning (or design) was used for the real effluent. The volume of hydrogen peroxide (Vetec®, 30%) added to the sample was estimated from the total organic carbon (TOC) concentration, and the amount of iron was based on the amount determined by the current Brazilian environmental legislation (CONAMA 430/2011) for effluents, which is equal to 15 mgL⁻¹. The aqueous solution of the dye studied had no iron; heptahydrate ferrous sulphate (FeSO₄·7H₂O) was added, P.A – ACS

dynamics. Table 1 shows the levels of each variable that was investigated in the factorial design.

Table 1 Matrix of the 2³ factorial design for evaluate dye degradation using the solar photo-Fenton process

Variables	Levels	
	-1	+1
t (min)	30	90
H ₂ O ₂ (μL)	600	900
Fe (mg)	0.2	0.4

After each assay, sodium sulfite (Na₂SO₃ - ACS Dynamic) was added in a stoichiometric proportion with the hydrogen peroxide, to inhibit the continuity of the reaction. Before analysis, the sample was filtered using a 0.45 μm membrane. In the case of the real effluent, the sample was collected before the physicochemical treatment used in the industry, and the tests were performed in a similar manner to those employed for the solution of the Drimaren red LC-5B dye, used in the previous tests.

2.3 Toxicity Tests

The acute toxicity of the liquid effluent was estimated through bioassays with lettuce seeds. The lettuce seeds of the variety *Lechuga simpson (Lactuca sativa L.)* were subjected to the diluted samples from the photo-Fenton process, with concentrations of 1%, 3%, 30% and 100%, using as support medium Petri dishes and filter paper [25]. Ten (10) seeds were used for each Petri dish. Subsequently, 5 mL of the effluent were added for each concentration tested in duplicate. Distilled water was used as negative control for toxicity. The results were expressed based on the average growth of roots (cm), Relative Growth Index (RGI) and Germination Index (GI).

The degree of toxicity of the sample was evaluated through the germination index (GI), which is the relation between the average length of the seeds, expressed by the Relative Growth Index (RGI), and the average of seeds that germinated. The RGI is the average growth of the radicle in the trial period. The growth rate of the radicle is given by Eq.(2) and the germination rate is given by Eq.(3) [26].

$$RGI = \frac{GRS}{GRNC} \quad (2)$$

$$GI = RGI \times \frac{SGS}{SGC} \times 100 \quad (3)$$

In the equations, GRS means the growth of the radicle in the sample and GRNC is the growth of the radicle in the negative control. SGS is the number of seeds that germinated in the sample and SGC is the number of seeds that germinated in the control. The methodology took into account the number of seeds that germinated and the length of the roots for a specified time. The seeds were incubated for seven days at 20 ± 1 °C. The amount of seeds that underwent protrusion and the elongation of roots were measured, considering germination as a growth equal or superior to 2 mm [27].

3. Results and Discussion

The solution of the dye was submitted to three processes: (1) photolysis; (2) reaction with peroxide and artificial white light; and (3) reaction with peroxide, iron, artificial white light (photo-Fenton) and sunlight. On the other hand, the real effluent, which was collected before the physicochemical treatment, was submitted only to the photo-Fenton process with sunlight.

3.1 Study of Degradation of Drimaren Red CL-5B Dye

As in Table 2, the dye solution was characterized according to values of pH, concentration, chemical oxygen demand (COD) and total organic carbon (TOC).

Table 2 Dye solution characterization

pH	Concentration (mgL ⁻¹)	COD (mg O ₂ /L)	TOC (mg C/L)
3.23	1000	1763.4	213.0

3.2 Photolysis of Drimaren Red CL-5B Dye Solution

Qualitatively, the study observed that there was no color change in the dye solution, discarding photolysis as a treatment for the studied solution. This result is corroborated in the literature, as the direct photolysis of most textile dyes may be difficult or very slow because such compounds are resistant to degradation by exposure to UV radiation [28]. A study of

the photolysis of the red dye, with concentrations ranging between 1×10^{-4} molL⁻¹ and 5×10^{-5} molL⁻¹, showed that the degradation of the dye decreased with increasing concentration [29]. Here, the concentration of the Drimaden red dye was 8×10^{-4} molL⁻¹ and we didn't observe degradation. Therefore, the photolysis was inefficient in this case.

3.3 Hydrogen Peroxide and Artificial Light Assay

The effect of the degradation of the dye solution was evaluated in an experiment that used only hydrogen peroxide and light. In this experiment, the reaction time was 60 min. and the amount of peroxide used was 750 µL. The experiment was performed in triplicate, and an average degradation of 9.37% was observed with a standard deviation of 0.58%. The appearance of the samples after the tests also indicated that the process was inefficient, since the color of the solution remained virtually unchanged.

3.4 Photo-Fenton with Artificial Light Assay

Table 3 shows the percentage of degradation and the reduction in TOC for each entry of the experimental assay. The addition of iron salts or iron oxides increased the efficiency of the Fenton or photo-Fenton reaction, because the iron acted as a catalyst and increased the speed of reaction [30]. After the tests, the amount of residual peroxide was measured with colorimetric test strips (peroxide test), which change color according to the amount of peroxide.

Table 3 Results of the mineralization of solution after photo-fenton process with artificial and sunlight

Entry	H ₂ O ₂ (µL)	Iron (mg)	Time (min)	TOC (%) (artificial light)	TOC (%) (sunlight)
1	900	0.4	90	73.97	91.74
2	600	0.4	90	74.33	94.12
3	900	0.2	90	72.85	93.01
4	600	0.2	90	72.27	87.41
5	900	0.4	30	51.63	87.76
6	600	0.4	30	41.07	79.42
7	900	0.2	30	51.68	73.87
8	600	0.2	30	59.65	88.91

Fig. 3 shows Pareto's chart built from data matrix presented in Table 3. None of studied variables showed statistical significant for mineralization, measured by TOC. Therefore, to perform the assays, using the real effluent, we used the values employed in the entry 2 which presented the best resulted for mineralization.

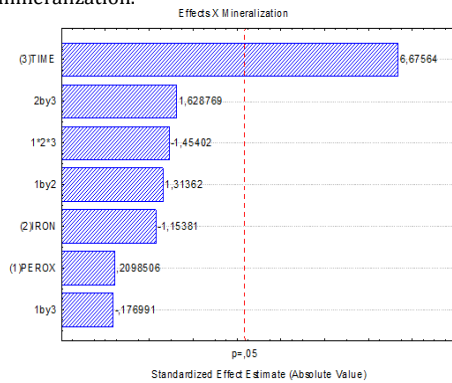


Fig. 3 Pareto chart for the analysis of the effects of the factors on the mineralization of the dye after treatment of photo-Fenton with artificial light.

3.5 Chemical Oxygen Demand of Aqueous Solution after Treatment Photo-Fenton with Artificial Light

The result of reducing the chemical oxygen demand (COD) was obtained from the experimental condition that presented the best mineralization of the aqueous solution of the dye (Entry 2). The COD values before and after treatment by photo-fenton process, using artificial light, are shown in Table 4.

Table 4 Results of chemical oxygen demand assay

Sample	COD (mg de O ₂ / L)	Reduction
Before treatment	1763.4	
After treatment	470.00	73.34%

A study using the Mordant Red 73 Azo dye showed that for degradation by photo-Fenton process, the COD reduction was 85% in 180 min of experiment for a dye concentration of 0.1 mM [31]. Herein, when we use a concentration of 0.94 mM of the Drimaren Red LC-5B dye in 90 minutes of experiment, a reduction of 73.34% was achieved for the COD. When was used solar photo-Fenton process, the best results presented values higher than 80% for COD. These results are summarized in the Table 5.

Table 5 COD after Solar Photo-Fenton proces

Entry	COD initial (mg O ₂ /L)	COD (mgO ₂ /L)	Reduction (%)
1	1763.4	237.7	86.52
2	1763.4	1211	31.30
3	1763.4	256.5	85.45
4	1763.4	324.0	81.63
5	1763.4	1014	42.50
6	1763.4	1092	38.03
7	1763.4	346.5	80.35
8	1763.4	711.5	59.65

These COD values indicate that there is significant reduction after use of solar photo-Fenton process. The reduction in COD was higher in assays of 90 minutes; therefore, time is an important factor in this result, indicating that there was a reduction in the organic matter and increase in the mineralization.

3.6 UV-Vis Spectrophotometry

Fig. 4 shows the UV-Vis spectrum of Drimaren red LC-5B dye solution. The maximum absorption was observed at 545 nm.

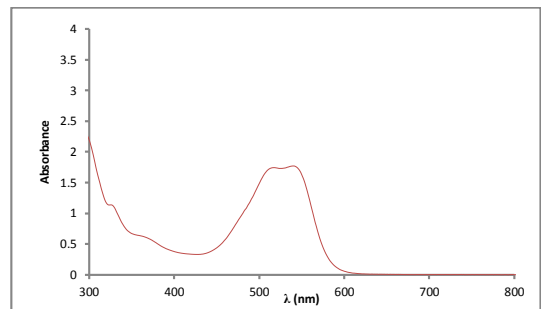


Fig. 4 UV-Vis spectrum of the Drimaren red LC-5B dye solution.

Table 6 shows degradation percentage of dye, obtained from UV-Vis spectra, when H₂O₂ and UV light only were used. This process was inefficient, resulting in strongly coloured solutions. For obtain the spectra, the samples were diluted at 1:10 ratio.

Table 6 Degradation assay of the dye solution after 1 h of exposure at peroxide (750 µL) and UV light in the absence of iron

Sample	Degradation (%)
1.1	9.70
1.2	9.70
1.3	8.70

This result demonstrates that the absence of iron (catalyst) does not allow the degradation of the dye at the maximum time of 90 min. and this is an indication that the chemical structure of the dye was not affected in the treatment with peroxide and UV light only (Fig. 5).

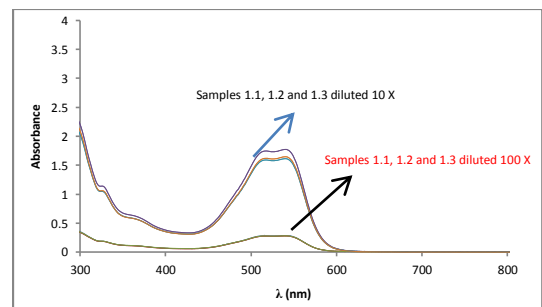


Fig. 5 UV-Vis spectra of the tests performed only with H₂O₂/UV

After treatment with the photo-Fenton process, using artificial light, the treated solutions were submitted to analysis by UV-Vis spectrometry. Fig. 6 shows these spectra.

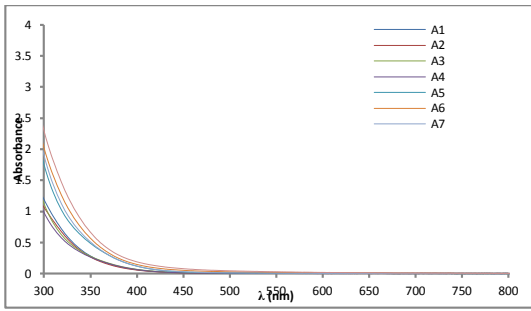


Fig. 6 UV-Vis spectra of seven solutions after photo-Fenton process, using artificial light

Fig. 7 presents an analytical curve that was built to quantify o dye remaining in the solutions. The results are presented in the Table 7.

Table 7 Quantification by spectrophotometry of the degradation of the model effluent after photo-Fenton treatment using artificial and sunlight

Entry	H ₂ O ₂ (μL)	Iron (mg)	Time (min)	Degradation (%)	
				Artificial light	Sunlight
1	900	0.4	90	61.11	62.77
2	600	0.4	90	59.68	61.46
3	900	0.2	90	59.08	68.49
4	600	0.2	90	59.56	71.94
5	900	0.4	30	58.85	71.58
6	600	0.4	30	56.11	82.18
7	900	0.2	30	55.51	95.15
8	600	0.2	30	49.56	63.01

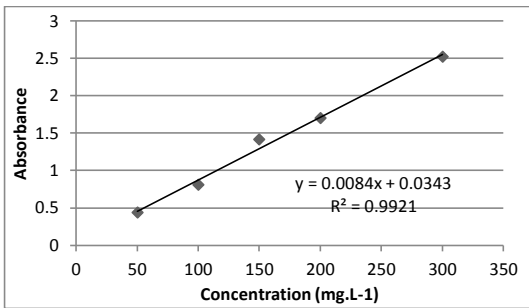


Fig. 7 Analytical curve (λ = 545 nm) to quantify the degradation dye after photo-Fenton process

Fig. 8 shows the Pareto chart, indicating the factors that are statistically significant, being the time the most relevant. Also, the interactions among the factors are significant, being the most important the interactions between the amounts of iron and peroxide, and between the amount of peroxide and the time. Only the interaction between peroxide and iron showed no statistical significance (Fig. 8).

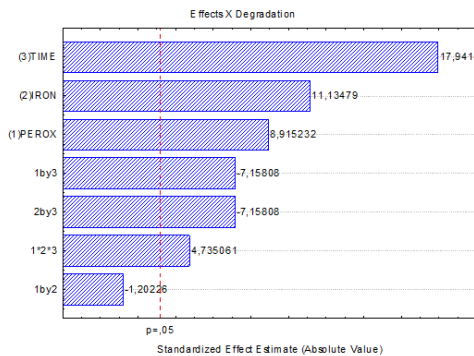


Fig. 8 Pareto chart to analyze the effects of factors on the degradation of the dye after photo-Fenton treatment with artificial light.

3.7 Toxicity of Aqueous Solution after Photo-Fenton Treatment with Artificial Light

The toxicity test with lettuce seeds was conducted in the assay that most mineralized the effluent. The results of germination and average growth of the seeds are expressed in (Table 8).

Table 8 Average number of seeds that germinated and average radicle growth

Seed	H ₂ O	BT*	AT**1%	AT3%	AT30%	AT100%
Germination	8.0	7.5	10.0	10.0	10.0	0.0
Growth radicle (cm)	2.2	1.8	2.3	2.1	1.3	0.0

*BT - Before of treatment; ** AT - After of treatment

It is possible to note that germination after treatment, when the effluent concentrations were equal to 1%, 3% and 30%, was higher than that observed for the negative control (distilled water), indicating that the process' products do not have enough toxicity to impede the germination of lettuce seeds at the concentrations tested (Table 8). However, when the assay was performed with the crude effluent (100%), no seed germinated, indicating the need for dilution to minimize the toxic effect. Root growth in the effluent before treatment was less than the growth observed for the negative control. Assays containing 1%, 3% and 30% showed a reduction in toxicity regarding the lettuce seeds, since they showed values close to those observed for the negative control. However, the average growth decreased at higher concentrations, indicating that the products – when more concentrated – do interfere in the growth and germination of the seeds. A more detailed analysis was performed based on the relative growth index (RGI) and germination index (GI), described in Eqs.(6) and (7). The graph in Fig. 9 shows that regarding lettuce seeds, there was better germination and greater root growth after treatment of the effluent. The chart also shows that, starting from the concentration of 1%, there is a decrease of both germination and root growth, although at the concentration of 30% germination is considered optimum [32]. However, it is important to note that the effluent when released into the water body undergoes dilution; this resembles the conditions of toxicological tests and with effluent concentrations of less than 100% the root growth is similar to the negative control.

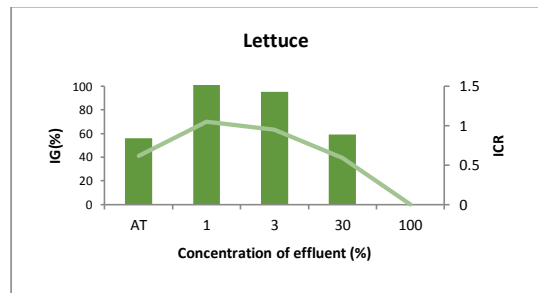


Fig. 9 Graph of GI values (%) in relation to RGI

3.8 Results Obtained for the Real Effluent after Treatment with the Photo-Fenton Process with Sunlight

Figs. 10 and 11 show UV/Vis spectra of the samples of the crude effluent and of the assays of the factorial design, respectively. A significant reduction in absorption can be observed after the treatment.

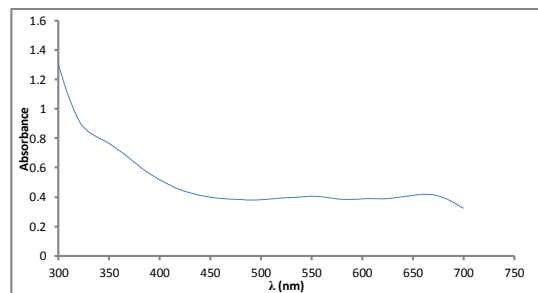


Fig. 10 Absorption spectrum of the raw effluent

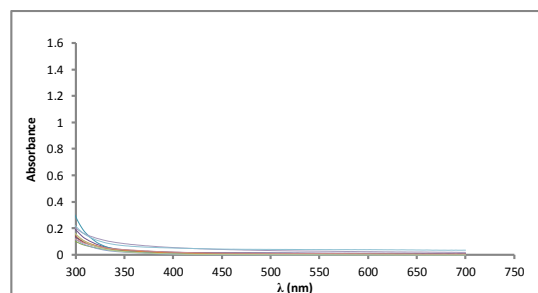


Fig. 11 Absorption spectrum of the experimental assays after photo Fenton treatment with sunlight.

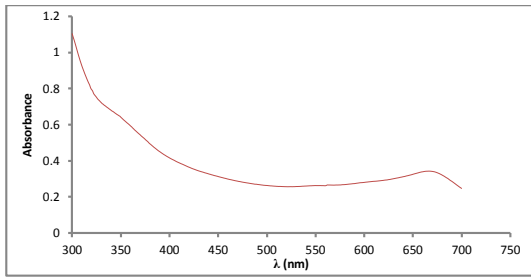


Fig. 12 Absorption spectrum of the crude effluent from the second collection

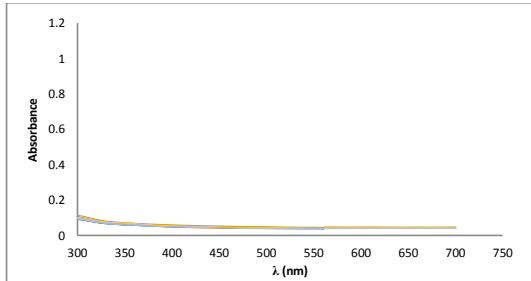


Fig. 13 Absorption spectrum of tests carried out in duplicate, of the crude effluent from the second collection after photo-Fenton treatment with sunlight.

Collections were carried out again at the real effluent, five months after the first sample collection and subjected to the same spectrophotometric tests in order to verify the reproducibility of the treatment with the photo-Fenton process with sunlight. In this new test, a 2³ experimental test was conducted in duplicate. The UV-Vis spectra are shown in Figs. 12 and 13.

3.9 Results Obtained after Treatment of the Real Effluent

The real effluent was subjected to the same experimental conditions as the aqueous solution of the dye when subjected to the photo-Fenton process with sunlight. The effects of the reduction of color, turbidity, COD and TOC are shown in (Table 9). The treatment proposed for the real effluent with the photo-Fenton process with sunlight allowed the removal of 84.26% to 98.46% of turbidity, of 85.89% to 89.60% of color, of 52.62% to 76.77% of COD, and 20.40% to 70.23% of TOC. When comparing the values of COD and turbidity among the treatments, the study observed that while the laundry reduces only 4.92% of turbidity, the proposed method reduces 98.46%. Regarding the COD, the laundry reduces 35.48% while the proposed process removes about 70%. The oxidation of textile dyes carried out by Lucas and Peres (2006) shows that the percentage of degradation by the photo-Fenton process is higher than the percentage of mineralization, represented by the TOC, which is corroborated by this study [33].

Some authors studied the efficiency of color reducing and COD of a textile effluent after treatment with the anaerobic process; the effluent was treated in an upflow anaerobic reactor. They achieved the maximum reduction of 30% and 71% for color and COD, respectively [32] – while the present study achieved the reduction of 89.1% and 69.3% for color and COD, respectively, using the photo-Fenton process.

The degradation of the real effluent by the photo-Fenton process with sunlight was evaluated statistically using *Statistica*® software. The response variable used was the result of the mineralization by the total organic carbon (TOC). To evaluate the effects of the factors and the interaction of these effects, the Pareto chart was used (Fig. 14).

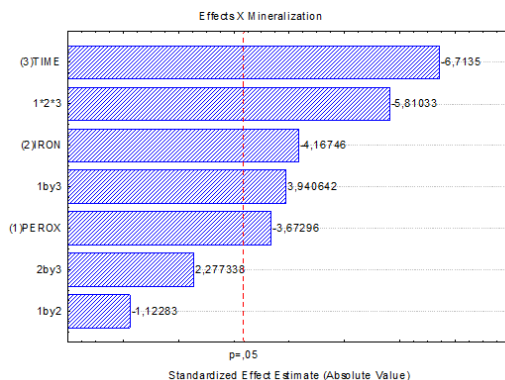


Fig. 14 Pareto chart – Effects of the variables studied in the treatment of the real effluent through the photo-Fenton process with sunlight.

Table 9 Results of the real effluent before and after the photo-Fenton treatment with sunlight

Real Effluent	Sample	Reduction (%)			
		COD	Turbidez	TOC	Color
Treated		35.48	4.92	-	-
	1	64.44	98.46	20.40	87.62
	2	69.82	97.60	36.71	88.12
	3	69.28	97.04	41.99	89.11
	4	67.14	84.26	24.37	85.89
	5	16.06	94.43	35.83	87.13
	6	53.87	94.59	42.99	88.12
	7	52.62	95.57	40.13	89.60
8	76.77	94.75	70.23	87.13	

The effects of weather, iron and peroxide, as well as the effects of the interaction of the three factors and the interaction of peroxide with time, are statistically significant in relation to mineralization, at a confidence level of 95%. The studied laundry only managed to reduce 35.48% of COD, while in this study the maximum reduction for the real effluent was 76.77%. In terms of turbidity, the treatment system used in the studied laundry reduced it only 4.92%, while in this present study the maximum reduction in turbidity reached 98.46%.

3.10 Analysis of Toxicity of the Real Effluent Treated with the Solar Photo-Fenton Process

The real effluent treated with the solar photo-Fenton process showed low toxicity in relation to the bioassays carried out with lettuce seeds. The test showed that the seeds germinated in the treated effluent with the sample *in natura* as well as with dilutions at concentrations of 30%, 3% and 1% (Table 10).

Table 10 Average number of seeds that germinate and average root growth (in cm).

Seed	H ₂ O	BT**	AT**1%	AT3%	AT30%	AT100%
IG (%)	9.0	0.0	7.5	10.0	8.0	9.0
ICR (cm)	6.2	0.0	6.6	6.6	5.8	4.5

*BT - Before of treatment; **AT - After of treatment

The study showed that prior to the treatment of the real effluent no seeds germinated, however, at all concentrations, including the negative control, there was germinating of virtually all seeds in the tests (Table 10). An important fact is that there is no need for dilution of the effluent after treatment, the real effluent treated showed no toxicity for the environment. Here, germination is considered as having root growth greater than 2 cm [33].

A more detailed analysis of the toxicity test, which shows the relative growth rate and the germination index before and after the treatment, shows that the effluent *in natura* is toxic to the *Lactuca sativa* seed; the treatment with the photo-Fenton process reduced the toxicity of the treated effluent, diluted and undiluted. A germination index above 55% is considered optimal. In the test, all the germination indexes obtained were above 80% [31]. The toxicity results obtained with the real effluent after treatment with the solar photo-Fenton process show that disposal in a water body does not affect aquatic life, due to the low toxicity observed.

4. Conclusion

Based on this present study, the following conclusions were obtained: the photo-Fenton process allowed dye degradation in the aqueous solution, obtaining a mineralization of 74.33% and 94.12% for the treatment with artificial and natural sun light, respectively. The photo-Fenton process was efficient in changing physicochemical parameters with results of removal of up to 98.46% turbidity and 80.60% of color. The toxicity test with lettuce seeds showed high toxicity of the real effluent before the treatment, and a clear increase in the relative growth rate and the germination index after the treatment, demonstrating that the proposed treatment reduced the toxicity of the effluent – this indicated that the resulting by-products were not toxic for the environment, considering the seeds tested. The statistical studies applied to each treatment showed that from the investigated factors, the one that most influenced degradation was time.

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